

**The 3<sup>rd</sup> International Conference on Environmental  
Disaster and Emergency Response Conference**

**National Yunlin University of Science and Technology (NYUST)  
Touliou, Yunlin, Taiwan, November 15-18 2005**

**Kinetics-based simulation –  
how can this approach  
help when assessing  
reaction hazard?**

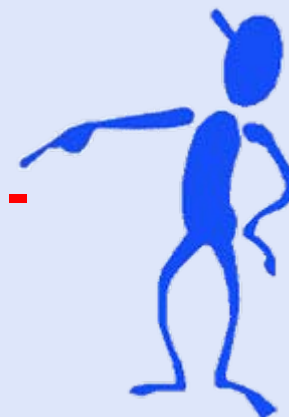
**A. Kossoy, ChemInform, St. Petersburg, Russia**

## *Thermal Hazards: Introduction*



### What is Thermal Hazard?

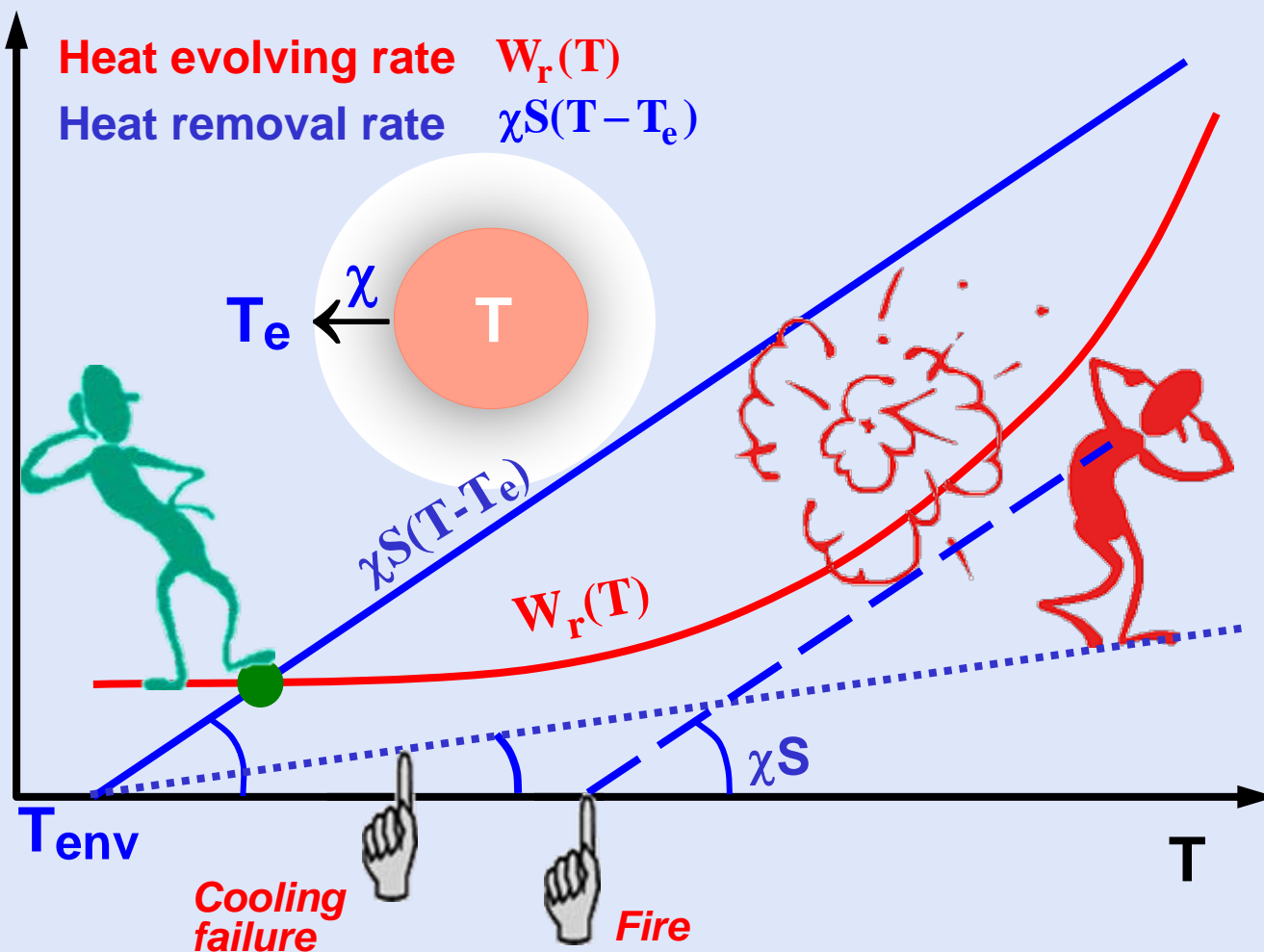
**Potential thermal (or reactive) hazard - reactive properties and physical conditions of a single chemical or mixture that have the potential to generate heat, gas product,...., that have the potential to harm**



### Main Sources of Thermal Hazards:

- ✓ **Synthesis reaction**
- ✓ **Instability of reactants and products (side reactions);**
- ✓ **Heat accumulation in a reactor;**
- ✓ **Pressure rise.**

## Thermal Hazard: Origins of Runaway



## Assessing Hazards: General Scheme



### Thermal Hazards of



#### Chemical Process

- ✓ Energy Potential and Reactivity of Reactants, Intermediates;
- ✓ Energy Potential and Kinetics of Synthesis and Secondary Reactions;
- ✓ Safety of Normal Process Mode;
- ✓ Accidents scenarios (cooling failure, fire, ...)
- ✓ Protection measures

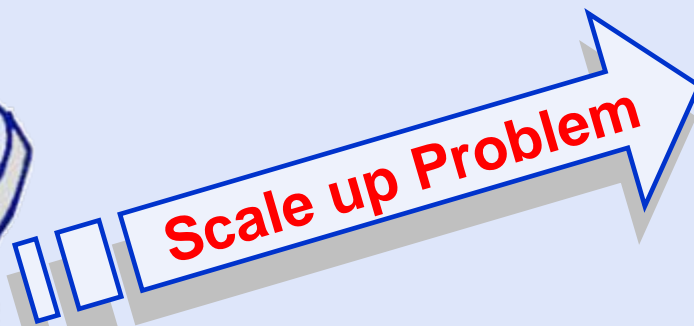
#### Chemical Product

- ✓ Energy Potential;
- ✓ Reactivity and Kinetics;
- ✓ Safe conditions of Use, Storage, Transportation;
- ✓ Accidents scenarios (fire, external heating, ...)
- ✓ Protection measures

## *Key Problem of Assessing Thermal Hazard*

### EXPERIMENTAL STUDY

- ✓ DSC, DTA,
- ✓ Heat Flow Calorimetry
- ✓ Reaction Calorimetry
- ✓ Adiabatic Calorimetry



HAZARD ASSESSMENT  
*of an Industrial Process*





## *Key Problem of Assessing Thermal Hazard*

### *The basic problem:*

**HOW TO PREDICT REACTION COURSE UNDER SOME CONDITIONS OF INTEREST?**

### *Can be solved either*

#### **BY USING CUSTOMARY METHODS**

-  **Methods are mostly based on simplest models**
-  **Qualitative or semi-quantitative results**
-  **Problems with scaling**
-  **Incomplete use of experimental data**

## *Key Problem of Assessing Thermal Hazard*

### *The basic problem:*

**HOW TO PREDICT REACTION COURSE UNDER SOME CONDITIONS OF INTEREST?**

**Or - IN GENERAL CASE UNDER ANY CONDITIONS**



**BY CREATING MATHEMATICAL MODEL OF A REACTION AND THEN**

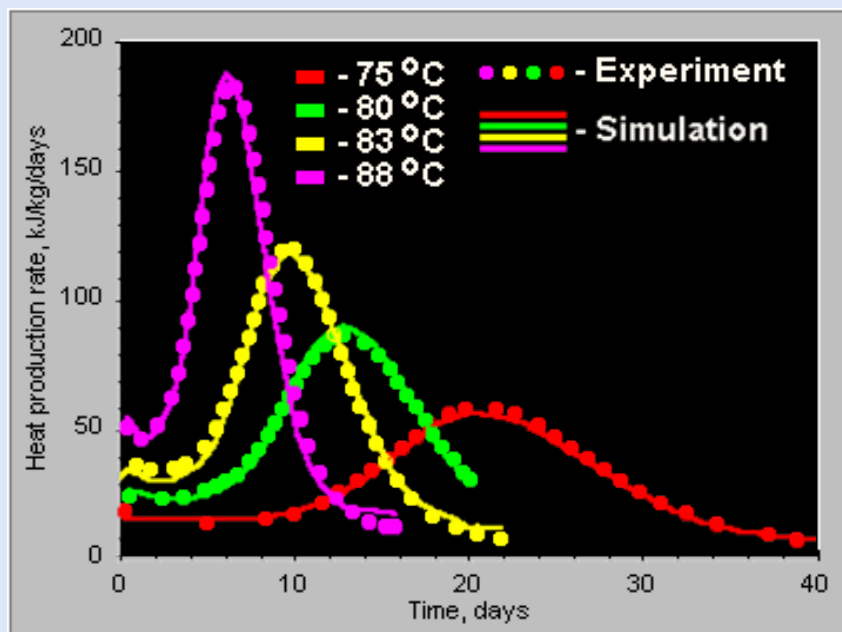
**BY SIMULATING PROCESS PROCEEDING**

## Some Examples: 1. Analyzing Reactivity

Aim: Revealing influence of various factors

Reaction: Decomposition of Cumene Hydroperoxide (CHP)  
(80% solution in Cumene (C))

Experiment: Heat flux calorimetry, simultaneous use  
of 4 isothermal data sets

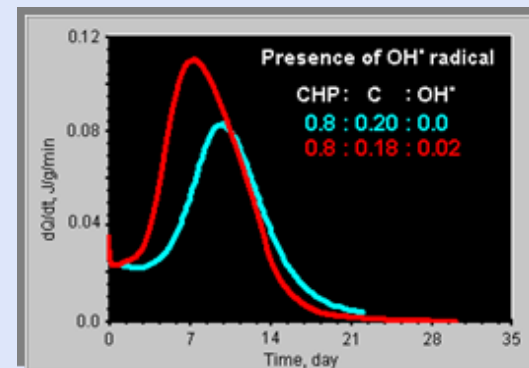
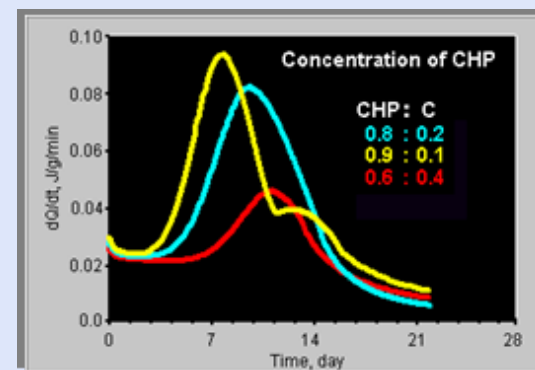
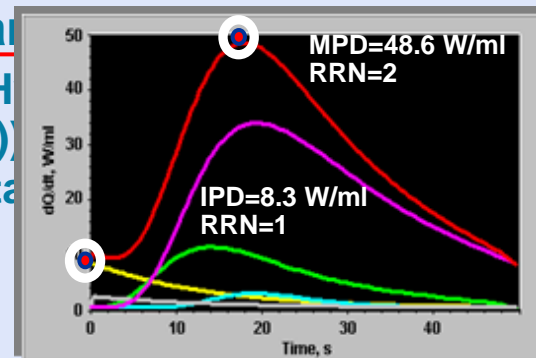
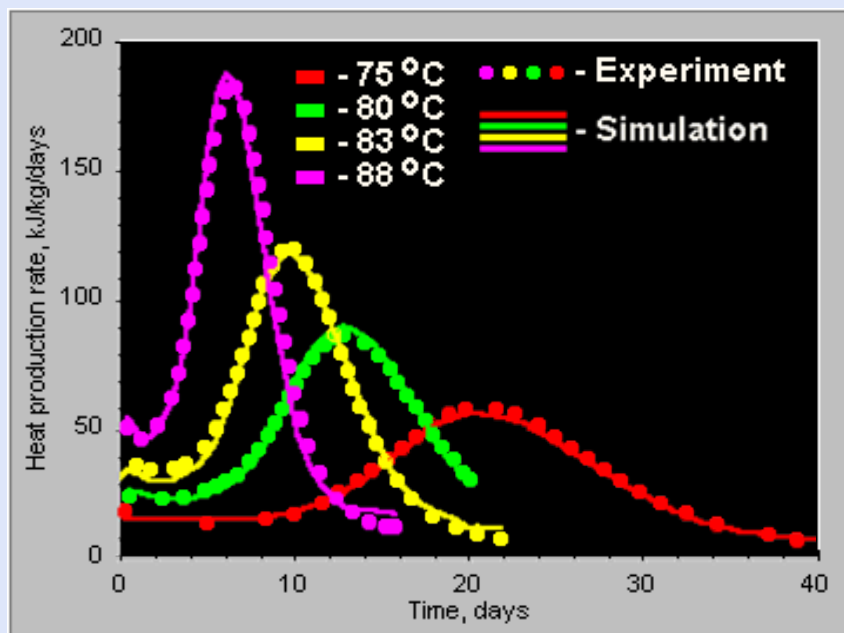


## Some Examples: 1. Analyzing Reactivity

Aim: Revealing influence of various parameters

Reaction: Decomposition of Cumene Hydroperoxide (80% solution in Cumene (C))

Experiment: Heat flux calorimetry, simulation of 4 isothermal data sets



## Some Examples: 2. Runaway & Vent Sizing

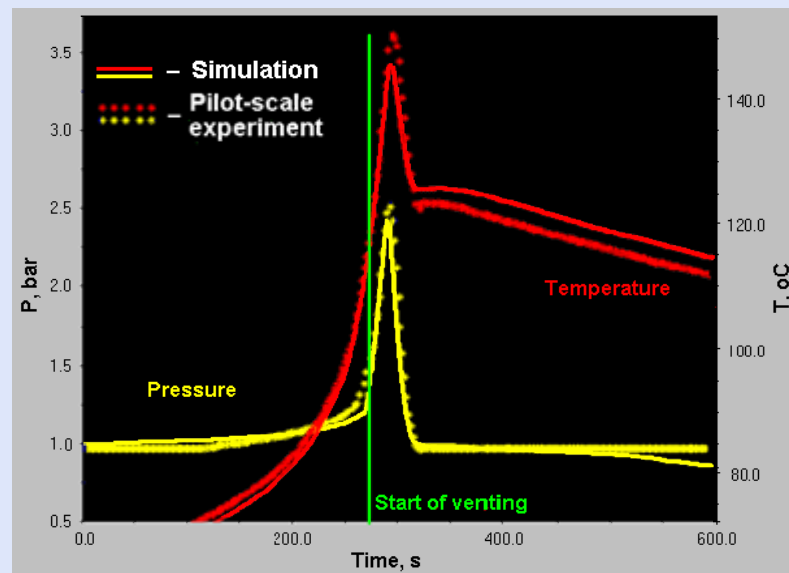
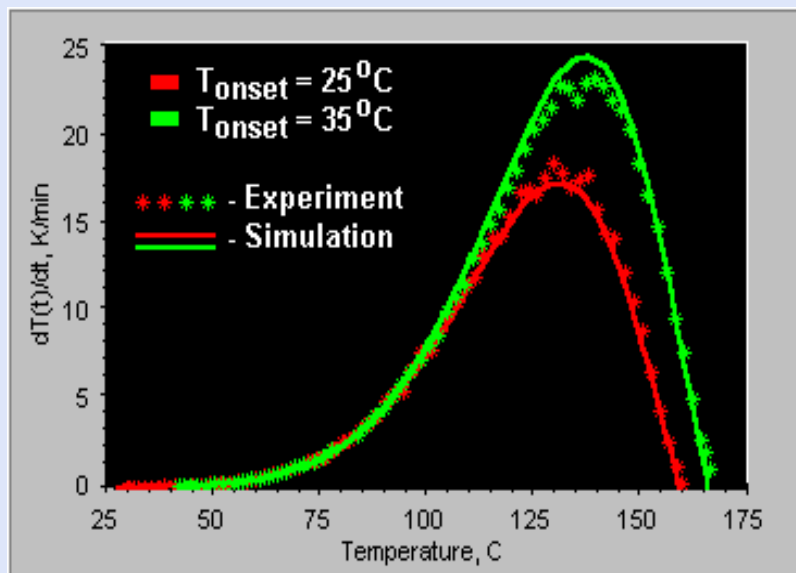
Aim: Verification of the software for ERS design,  
(HSE Round-Robin test)

Reaction:  $I + PA \rightarrow IP + PAc$

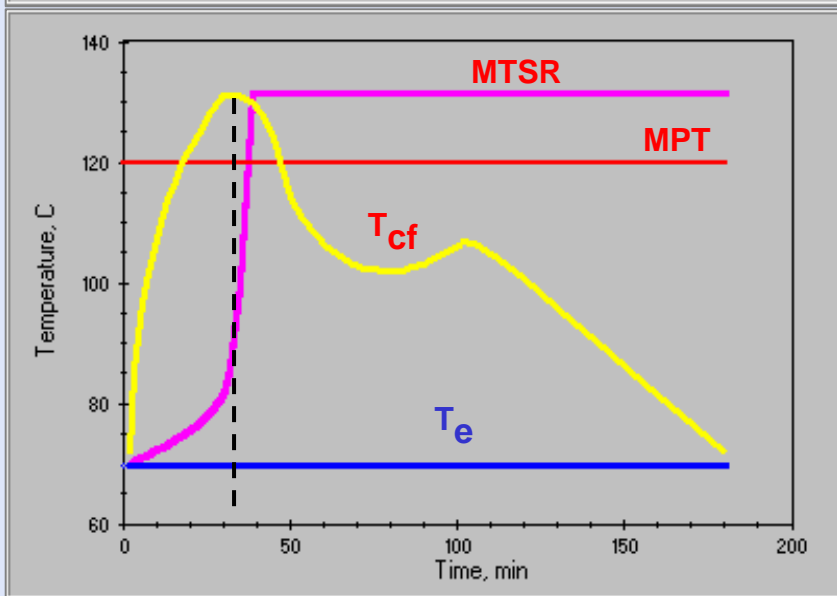
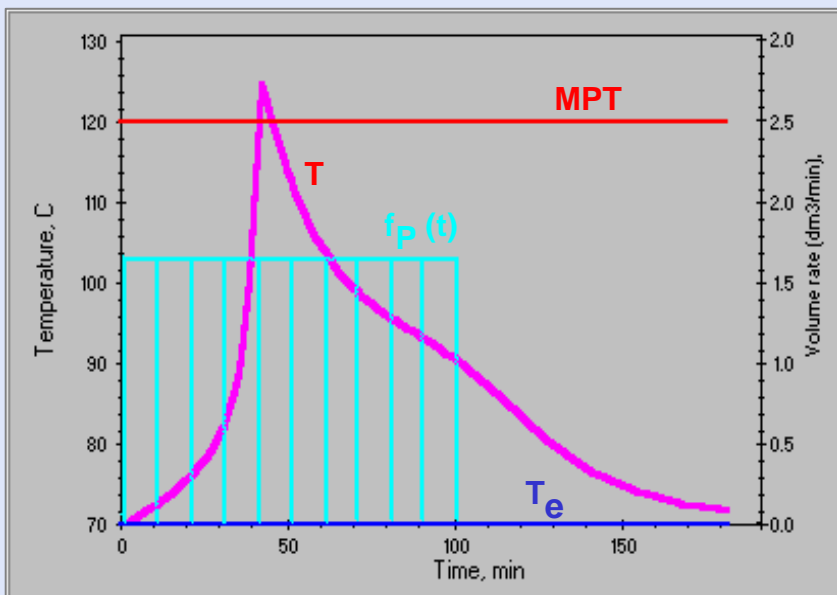
Experiment: Adiabatic Calorimetry; simultaneous use  
of 2 data sets: To 25 °C & 35 °C

Reactor: Vertical tank,  $V = 312$  liters;  $U = 270$  W/m<sup>2</sup>/K,  $S = 1.53$  m<sup>2</sup>

Vent system: Type: Valve; Position: Top; Length: 4.82 m; Diameter: 7 cm  
Actuation Conditions: Pressure 1.5 bar, Overpressure 5%;



### Example 3: Optimizing Semi-BATCH



#### 1. Optimization criterion - Inherent Safety

$\max(\text{MPT} - \text{MTSR}); \text{MPT} = 120 \text{ C}$

#### 2. Expediency and Engineering constraints: same as in Example 1

#### 3. Controls to be optimized:

$f_p(t)$  defined as Sequence of Pulses:

10 identical pulses:

distance (i) = 0 min	fixed
$f_p(t) = 1.65 \text{ dm}^3/\text{min}$	var
duration (i) = 10 min	fixed

#### Initial Mode (before optimization)

$T_e = 65 \text{ C}$ , initial filling - 100 l of P; feed of I until reaching equimolar composition

Normal mode:

$T_{\max} \approx 124 \text{ C}$

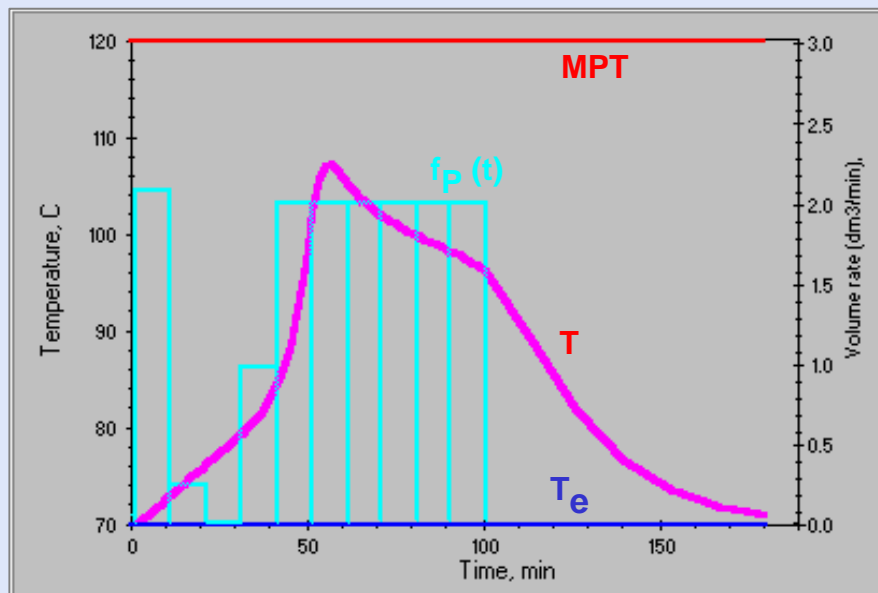
$t_{\max} \approx 42 \text{ min}$

Accident:

$\text{MTSR} \approx 132 \text{ C}$

$t_{cf \max} \approx 30 \text{ min}$

### Example 3: Optimizing Semi-BATCH



#### Optimized Normal Mode:

$$f_p = f_p(t)$$

$$T_{\max} \approx 107.5 \text{ C} ; t_{\max} \approx 57 \text{ min}$$

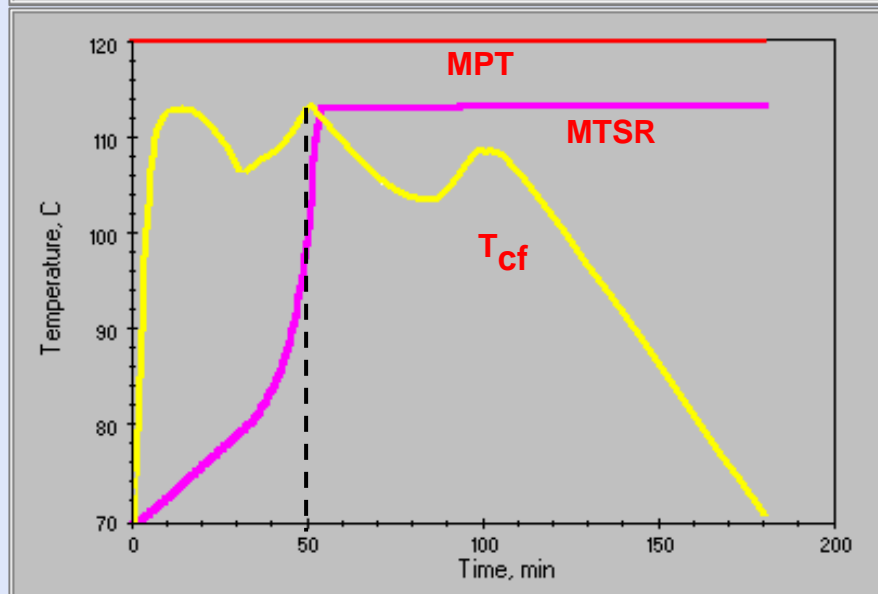
$$t_f \approx 170 \text{ min} \quad C_I(t_f) = 0.02$$

$$C_P(t_f) = 0.0003$$

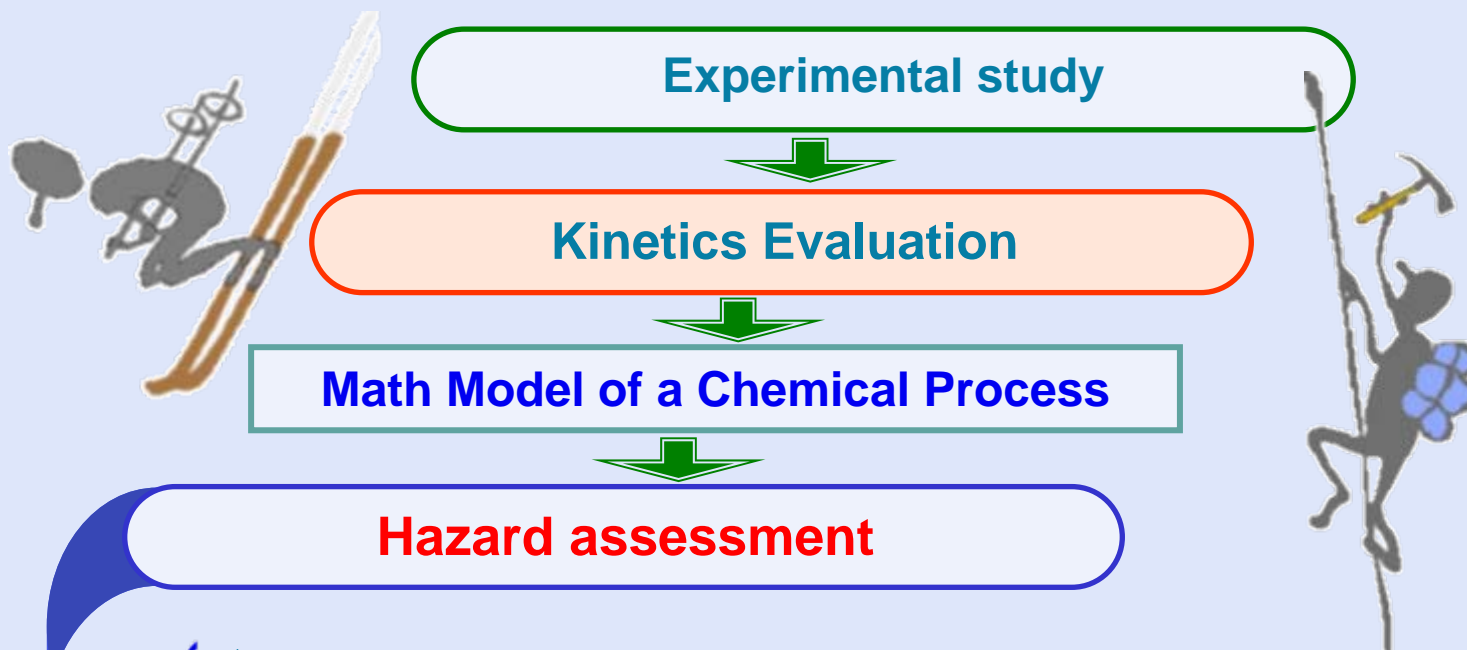
#### Accident:

$$MTSR \approx 113.3 \text{ C} ; t_{cf \max} \approx 50 \text{ min}$$

***Inherent Safety is provided***



## *General Approach to Assessing Hazard*



- ✓ Reactivity of a Material/Mixture
- ✓ Critical Conditions of Thermal Explosion
- ✓ Runaway in a Reactor and Design of Emergency Relief Systems
- ✓ Design of Inherently Safer Processes

## *Difficulties of introducing the Approach*



**A knowledge- consuming way:  
requires applying methods from  
various fields - mathematics,  
numerical methods, chemical  
kinetics, thermal physics, etc.;**






**Every step should be provided with the  
appropriate elaborate methods;**



**High demands have to be made to the  
professional skill of a researcher.**

## *Main merits of the approach*

-  Allows applying more adequate complex mathematical models of processes;
-  Allows investigating various scenarios of process proceeding;
-  Gives the principal solution of the scale-up problem.



## *How to simplify its use in practice ?*

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**By creating the problem - oriented tools that are convenient for Researchers and include relevant METHODS and the corresponding SOFTWARE.**



## *Thermal Safety System : Methodology*

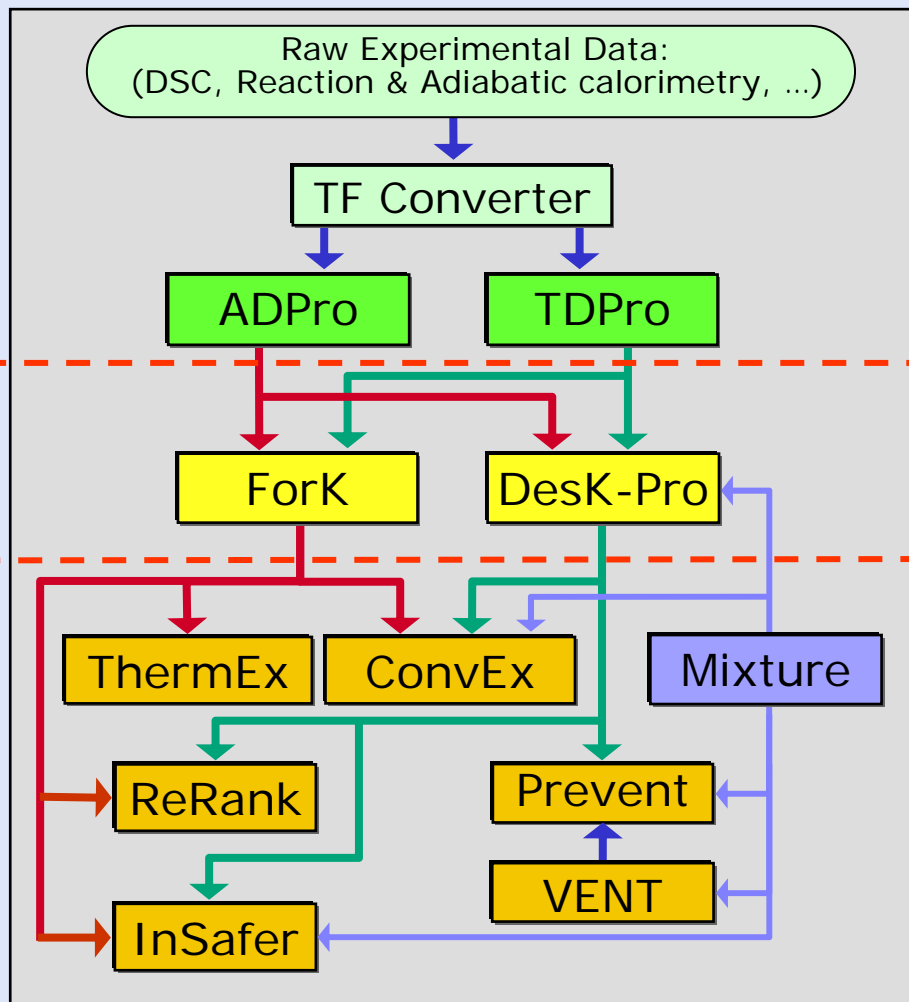
-  ***Up-to-date theoretical basis for:***
  - ✓ **Thorough processing of various calorimetric data;**
  - ✓ **Creation of mathematical models of chemical reactions;**
  - ✓ **Simulation of thermal explosion in solid and liquid substances;**
  - ✓ **Simulation of runaway in industrial reactors and Design of Emergency Relief Systems for protecting them**
-  ***Coordination of all the stages.***

## TSS– Tool for Hazard Assessment







Thorough processing  
of experimental data

Creation of math models  
of chemical reactions






Assessment or reaction  
hazards;  
inherent safety, runaway  
simulation





## *TSS – major features*

-  **Elaborate problem-oriented methodology as the basis;**
-  **Incorporation of mathematical methods with knowledge and intuition of a researcher into unified strategy;**
-  **The most relevant up-to-date mathematical methods for solving problems;**
-  **Possibility to process simultaneously results of different multi-response experiments;**
-  **Full interconnections and co-ordination between separate programs;**
-  **Unified elements of User's interface, flexible graphics**

## ***TSS: To Whom it is addressed***

-  **R&D Centers of Chemical and Pharmaceutical Companies;**
-  **R&D Centers of Manufacturers and Users of Explosives;**
-  **Consulting Firms dealing with Chemical Processes and Hazard Assessment;**
-  **Thermal-analytical Laboratories;**
-  **Chemical Engineering Departments of Universities**

## *Conclusions*

-  **The kinetics-based simulation is a very efficient method for solving such complex challenge as assessment of reaction hazards. Being free of essential simplifications this approach can be applied to a wide variety of practical problems**
-  **This approach is not for complete replacement of the traditional methods. Quite the contrary they mutually complement each other and simulation will be most helpful when the potential danger of a reaction or process has been revealed by using simplified empirical methods**